Designing for Efficiency: New Plants and Major Renovations

September 28, 2023





ILLINOIS SUSTAINABLE TECHNOLOGY CENTER PRAIRIE RESEARCH INSTITUTE

Who We Are

We assist buildings and communities in achieving energy efficiency, saving money, and becoming more sustainable.

We are an applied research program at University of Illinois.

Our goal: Reduce the energy footprint of Illinois and beyond.







ISTC Mission

To encourage and assist citizens, businesses and government to prevent pollution, to conserve natural resources, and to reduce waste to protect human health and the environment in Illinois and beyond.





About the IEPA PWI Energy Efficiency Program

The Illinois EPA Public Water Infrastructure Energy Assessment Program helps municipalities reduce the cost of water and wastewater treatment.

- NO-COST energy assessments and technical assistance
- Comprehensive report listing:
 - Cost of upgrades
 - Estimated payback period
 - Any applicable incentives or funding opportunities
- Operator continuing education events

Apply at: www.smartenergy.lllinois.edu/water





Funding provided in whole or in part by the Illinois EPA Office of Energy. This program is in partnership with the U.S. Dept. of Energy Sustainable Wastewater Infrastructure of the Future

(SWIFT) Accelerator for energy efficiency in wastewater treatment.



Energy Efficiency & Renewable Energy



Webinar Objectives

- 1. Recognize common-sense designs that reduce energy consumption
- 2. Identify hidden efficiency designs that improve operating efficiency
- 3. Review examples of plants that designed for efficiency
- 4. Discuss potential funding sources for resiliency projects





Designing WWTPs for Efficiency

Webinar Speakers



Shawn Maurer Technical Director SEDAC - UIUC





Amanda Streicher Asst. Wastewater Dept. Manager Baxter & Woodman



Apply for an Energy Assessment!

Step 1: Initial Application – Pre-Qualification

- Apply at <u>www.smartenergy.illinois.edu/water</u>
 - Be located in Illinois and be publicly-owned
 - Allow SEDAC/ISTC to visit site
 - Be willing to share facility information
 - Share final assessment report with Illinois EPA

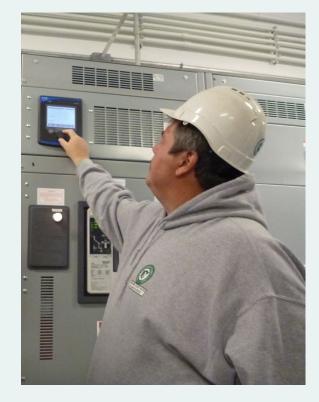
Step 2: Data Collection – We're here to assist!

- Facility information
 - Process flow diagram, types of processes, etc.
- 2 years of utility bills and DMRs

Step 3: Site Visit Scheduled



Step 4: Receive Comprehensive Report





Why Complete an Energy Assessment?

Existing System or No Previous Assessments? Identify missed opportunities Plan for capital improvements Uncover what is possible 3rd party support for personnel's ideas

New or Recently Upgraded?

Always more to improve

Plan for future opportunities outside the scope of recent projects

New technologies and processes always in development



Identify opportunities for repairs or upgrades and associated funding!



Keys to Designing for Efficiency

- Use Wastewater Data!
- Don't Fight Gravity!
- Minimize Recycle Pumping (fights gravity!)
- Optimize Pumping Staging
- Proper Equipment Sizing
- Employ Variable Speed Devices or Timer Systems
- Improved Aeration Controls
- Decouple mixing and aeration



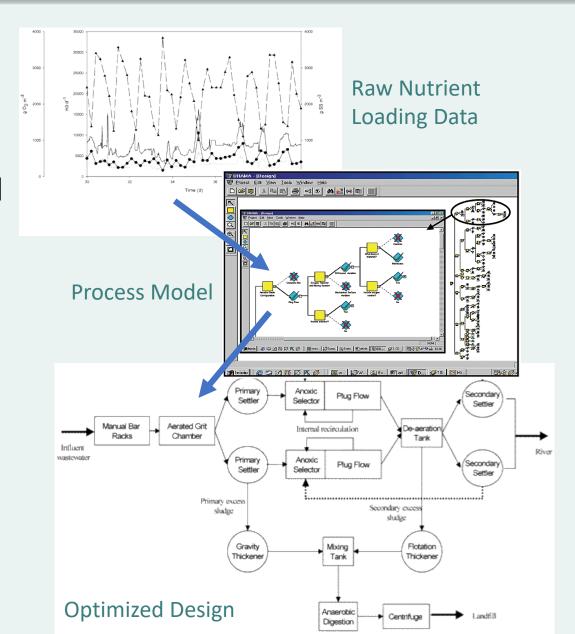


Using Wastewater Data

Nutrient removal coming for most plants! Requires more tuning and precision than planning for just BOD and ammonia removal

- Phosphorus and Nitrogen removal is coming for most plants!
- Knowing existing strength and flow profiles can better tune process.
 - 10 States or other design standards tend to overdesign for loading – better for future growth estimates





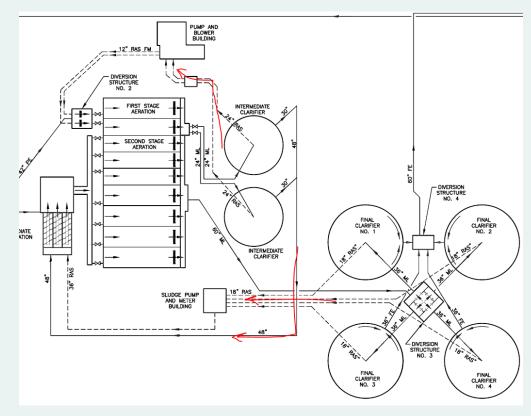
Don't Fight Gravity!



 Raised denitrification tower for storage space



Permanent increase in pumping head of 15-20ft!

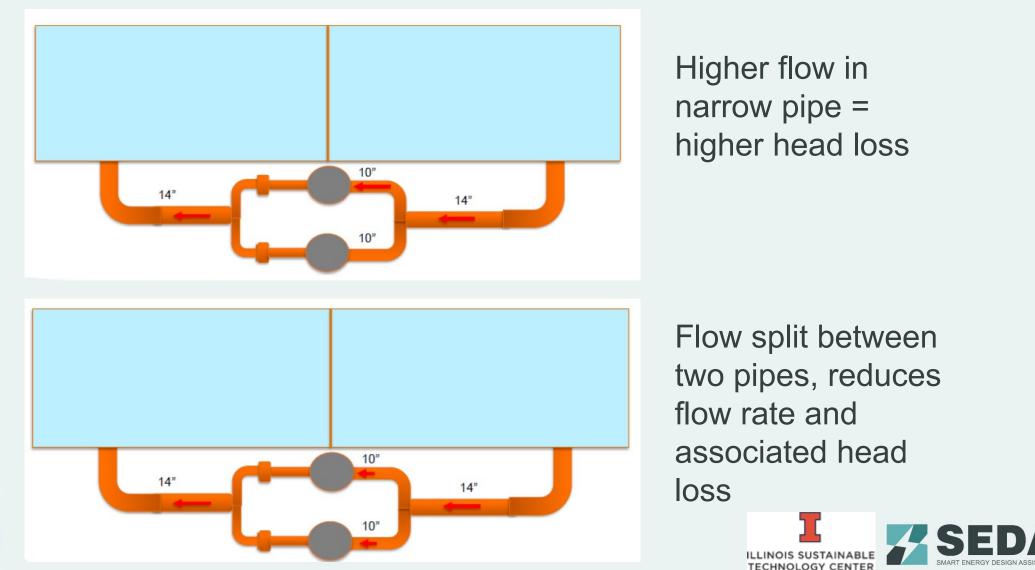


- Recycle-intensive process
 - 2 sets of RAS plus aeration

recycle!



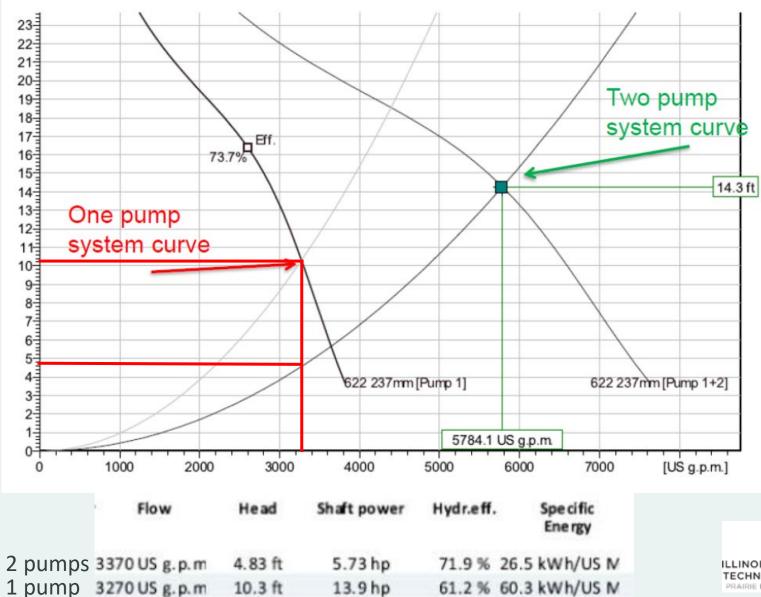
Optimize Pump Staging



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Optimize Pump Staging



NENTAL PRO

Annual Energy Consumption

1 Pump: 107.3 MWh/yr

2 Pumps: 47.4 MWh/yr

~\$6,000 annual savings at \$0.10/kWh

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Build-In Modularity – Size For Current Need



- 5 small blowers 2 operate under normal conditions
 - Remaining 3 are back-up + peak
 loading blowers.



- Two ditches, only 1 used most of the time
 - 2nd ditch for storm flows

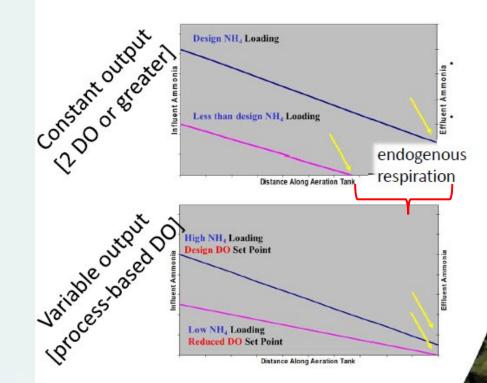




Consequences of Over-Sizing

Impacts of Aeration (DO

process implications



Improve biomass health

Less endogenous respiration

Improved biomass settleability

Maximize process unit performance

Increased process kinetics

Reduce aeration energy

Reduce process oxygen demand

Increase operating aeration efficiency







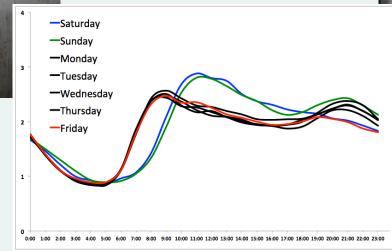
Content courtesy Randy Chann, EDI, Boone Co. RSD Chair

Employ Variable Speed or Timers



VFDs improve

modularity of equipment



Both help adjust for

diurnal loading



Timers are an excellent

lower-cost aeration

control measure





Optimizing DO Control

Only Add DO Needed for the

process

Chart indicates airflow reduction

possible from reducing DO

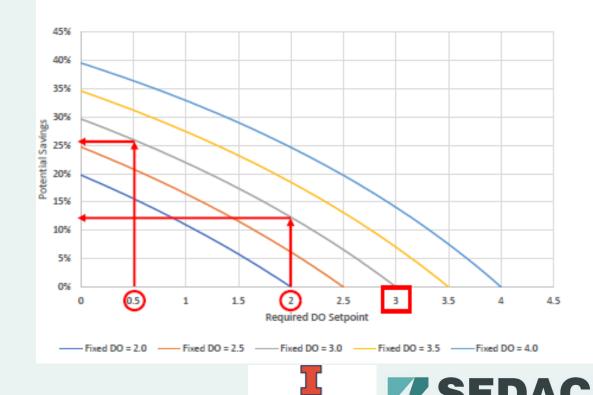
setpoint.

Employ DO Probes, blower VFDs, and automated basin flow valves

Cost of Over Aeration

Airflow Reduction Potential

(Operating Residual DO Concentration)





Content courtesy Randy Chann, EDI, Boone Co. RSD Chair

Improved Aeration Controls

Many operators manually balance airflow between basins

- Process tanks
- Aerobic digesters
- Tapering airflow in single basin

Modern Designs are more automated

- EBNR Processes
- SBR
- MBR
- MBBR
- SND basins





Controlling each basin

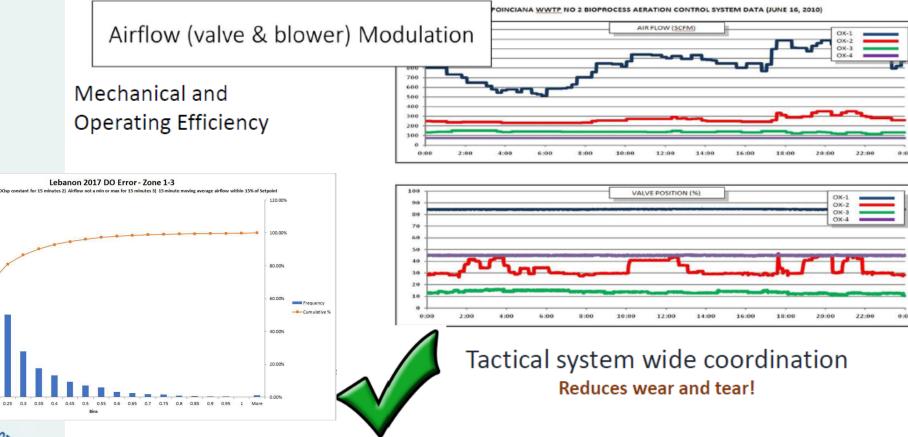
optimizes aeration demand



Aeration with Most-Open Valve Control

Toho Water Authority (Cyprus West WRF) 2010

Aeration DO Control





200000

180000

160000

120000

80000

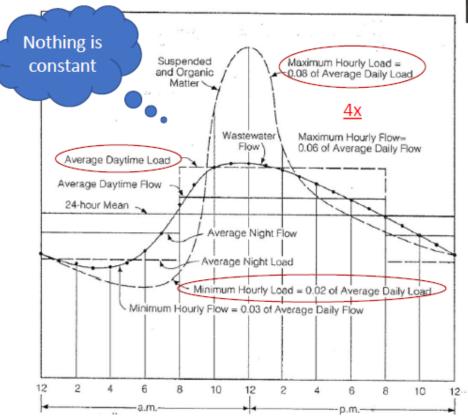
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Content courtesy Randy Chann, EDI, Boone Co. RSD Chair

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Optimizing Aeration Design

How do we run an activated sludge plant?



Impacts of Aeration

Aeration Constant vs Variable?

How do we operate the aeration system (blowers)?

Fixed Output		ing DO Tar n, % reduc	Variable Output			
Max Hourly Load	2	1 - 12%	0.5 - 16%	2		
Average Load	5.9	5.4	5.2	2 - 50%	1.5 - 53%	
Min Hourly Load	7.9	7.6	7.5	2 - 75%	1.0 - 78%	



Content courtesy Randy Chann, EDI, Boone Co. RSD Chair



Decoupling Mixing and Aeration



Decoupling Solutions

Add independent mixing capabilities [intermittent aeration, large bubble mixers, mechanical mixers]

 + reduces mixing energy
 + may be required for DO management



Content courtesy Randy Chann, EDI, Boone Co. RSD Chair





Shawn Maurer, PE, CEM spmaurer@illinois.edu 217-300-1771

WENTAL PR

ON AGE

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Amanda Streicher, Baxter & Woodman Designing for Efficiency at a WRRF

September 28, 2023



Agenda

- Proper Planning
- Education of Decision Makers
- Preliminary Design and Report
- IEPA required vs Actual Design Conditions

Large Energy Users

- Aeration and Activated Sludge
- Pumping
- Instrumentation and Automation
- Owner/Staff Support and Champion
- Question/Discussion

Proper Planning

□Planning is the First Step

□ Facility Planning Report

□ Facility Assessment (ComEd) – Very high level

Comprehensive Energy Assessment (ComEd

funded) – Detail Evaluation

SEDAC Assistance and Resources

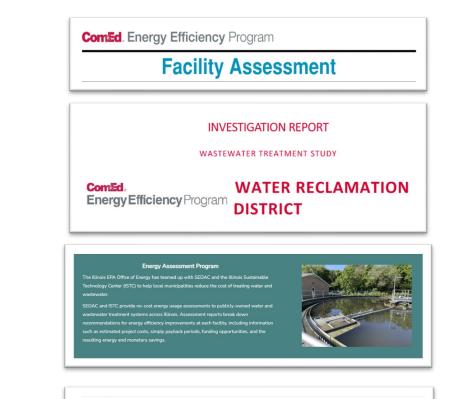
Master Plan

Include a section on Energy

□Identify big picture things to consider in design

Energy Neutrality Plan

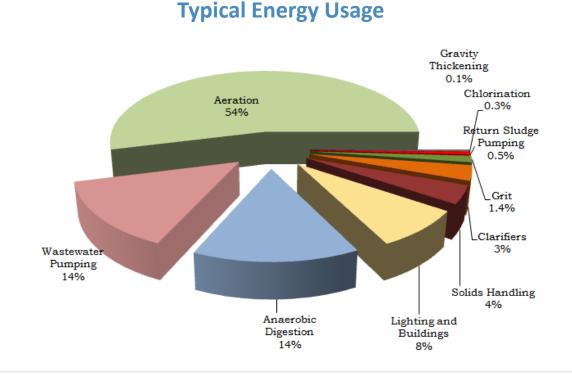
□ Focus specifically of energy usage



Master Plan for Process Capacity Buildout on the Facility's West Site

Education of Decision Makers

- **Communicate Plan and Goals**
- Show WRRF to Board or Trustees
- Energy Usage and Costs
- **Get Buy-in**



Preliminary Design and Report

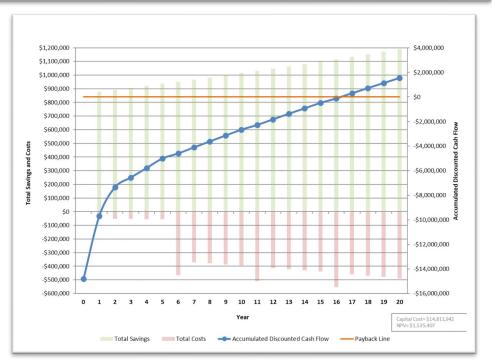
Equipment Evaluation

- Capital Cost
- Operating Efficiency
- Energy Usage
- O&M Requirements
- Chemical/Polymer Usage
- Operating Range

Life Cycle Cost

- Operation and Maintenance
- Major overhauls
- Establish total cost of Ownership

Diffuser	<u>SOTE Require</u>	ments	
SOTE	36%	40%	
Air requirement (scfm)	8400	7650	
Max air per blower (scfm)	2800	2550	
Quantity of blowers	4	4	
Blower HP	200	150	
			Difference
Blower Capital			
Neuros	\$ 817,564	\$ 645,800	\$171,764
ABS Sulzer	\$ 638,030	\$ 631,960	\$6,070
Diffusers Capital			
EDI	\$ 140,000	\$ 272,500	(\$132,500)
Sanitaire	\$ 200,000	\$ 290,000	(\$90,000)
Blower operating cost/year*	\$ 121,974	\$ 90,404	\$31,570
Cost wasted for air past mixing	(\$1,419)	(\$1,963)	(\$544)
*Using \$0.065/kWh			

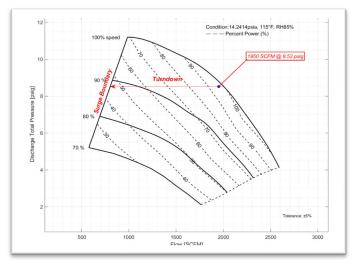


IEPA required vs Actual Design Conditions

IEPA Required vs Actual Operation Conditions

5-Day	Biochem	ical C	xygen De	emand (B	OD ₅)							IEPA Loa	ding	Actual Loading
P	Present co	ncent	ation									204	mg/L	16
	xisting lo				6000	00 PE	x 0.1	7 pp	d/PE =				lbs/day	8,00
A	dditional													
	2630	0 PE	c 0.17 ppd	BOD5/PE				_				4,471	lbs/day	4,47
S	destrean	n loadi	ng											
	Gravi	ty Bel	t Thickene	r Filtrate					BOD:TSS =	0.25		94	lbs/day	9
	Cent	rifuge	Centrate						BOD:TSS =	0.25	-	134	lbs/day	13
Т	otal BOD	5 loadi	ng						M			14,899	lbs/day	12,57
			concentrat	ion						1		207	mg/L	1

Operating Range



Make sure equipment selected can meat the IEPA requirements and operate efficiently at actual conditions

Large Energy Users – Aeration and Activated Sludge

• Diffusers

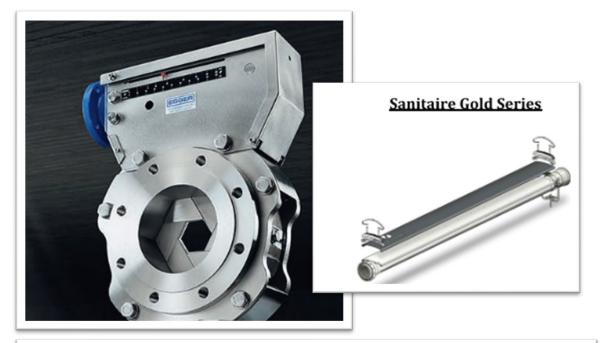
- SOTE is Critical
- Cleaning Requirements Fouling is re

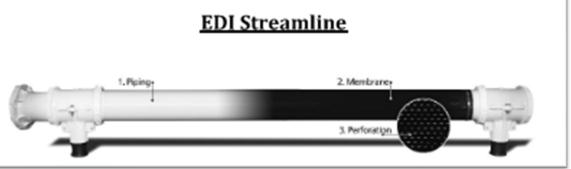
Air Control Valves

- Iris vs Butterfly
- Location Preferred on each drop pipe
- Actuated is needed to match process demand

• Blowers

- High Efficiency Turbo
- Screw Hybrid





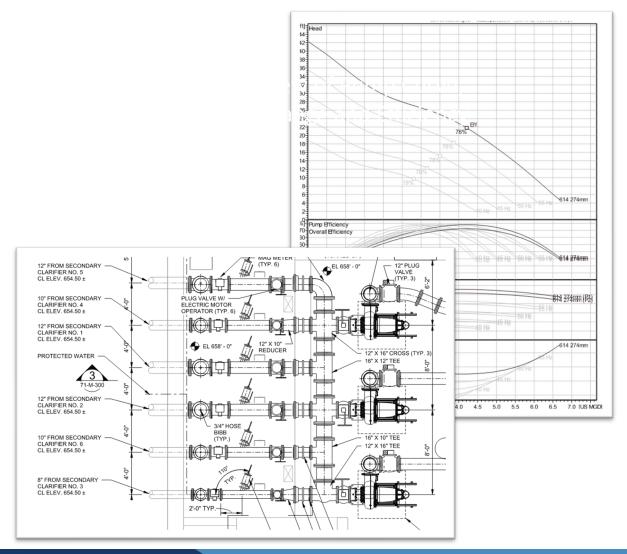
Large Energy Users – Pumping Systems

ODetermine Pump for the Process

oLiquid, sludge, or chemical

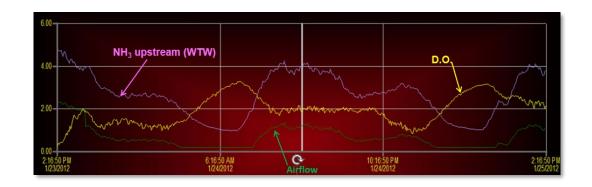
- **Provide VFD to match process**
- Consider RAS direct connection to Final Clarifiers

OReduce TDH by using WL in Clarifiers



Large Energy Users – Instrumentation and Automation

- DO, ORP, pH and Ammonia probes allow real-time understanding of the process
- Use Controls & Automation to reduce buffer
 - Could create risk for operators
 - Make sure to collaborate in design
- Incorporate Power Monitoring into MCCs & VFDs
- SCADA is critical for monitoring probes and energy usage
 - Phone and tablet access





Questions/Discussion

